

AMENDMENTS TO THE SPECIFICATION

Please insert in the first sentence after the title, the following new paragraph.

This application is the U.S. national phase of International Application PCT/EP2003/013818, filed November 25, 2003, claiming priority to European Patent Application Numbers 02080616.2 filed December 18, 2002, and 03101357.6 filed May 14, 2003, and the benefit under 35 U.S.C. 119(e) of U.S. Provisional Application Numbers 60/435,195, filed December 20, 2002, and 60/482,697 filed June 26, 2003; the disclosures of International Application PCT/EP2003/013818, European Patent Applications 02080616.2 and 03101357.6, and U.S. Provisional Application Numbers 60/435,195 and 60/482,692, each as filed, are incorporated herein by reference.

Please replace the paragraph beginning at page 2, line 15, and ending at line 19 with the following paragraph.

The present invention therefore relates to solid Lewis adducts comprising MgCl_2 , a Lewis base (LB) belonging to ethers, esters, ketones, silanes or amines and an alcohol ROH, in which R is a C1-C15 hydrocarbon group optionally substituted with heteroatoms containing groups, which compounds are in molar ratios to each other defined by the following formula $\text{MgCl}_2(\text{ROH})_m(\text{LB})_n$ in which m ranges from 0.05 to 6, n ranges from ~~0.08~~0.07 to 6.

Please replace the paragraph beginning at page 3, line 2, and ending at line 3 with the following paragraph.

Preferably n ranges from ~~0.07~~0.08 to 3, more preferably from 0.1 to 2.5 and especially from 0.5 to 2.

Please replace the paragraph beginning a page 3, line 20, and ending at line 28, with the following paragraph.

An alternative embodiment the adduct of the invention is obtained ~~in solid~~ in solid form by subjecting the molten adduct mentioned above to spray-cooling process. When this option is pursued it is preferred that in the first step the magnesium chloride, the alcohol and the electron donor compound be contacted to each other in the absence of an inert liquid diluent. After having been

molten the adduct is sprayed, through the use of the proper devices that are commercially available, in an environment having temperature so low as to cause rapid solidification of the particles. The cold environment can comprise a cold liquid or gas. In a preferred aspect the adduct is sprayed in a cold liquid environment and more preferably in a cold liquid hydrocarbon.

Please replace the paragraph beginning at page 12, line 21, and ending at line 27 with the following paragraph.

Into a 2 L four-necked glass reactor, equipped with a mechanical stirrer and a thermometer, purged with nitrogen, 1500 mL of TiCl_4 were introduced and cooled at 0 °C. While stirring, 60 g of microspheroidal adduct prepared above were added. Subsequently an amount of diisobutylphthalate corresponding to ~~0,125~~0.125 moles per mole of Mg, were added to the suspension. The temperature was raised to 100°C and maintained for 120 min. Then, the stirring was discontinued, the solid product was allowed to settle at 100°C for 15 minutes and the supernatant liquid was siphoned off.

Please replace the paragraph beginning at page 13, line 1, and ending at line 7 with the following paragraph.

Into a 2 L four-necked glass reactor, equipped with a mechanical stirrer and a thermometer, purged with nitrogen, 1500 mL of TiCl_4 were introduced and cooled at 0 °C. While stirring, 75 g of microspheroidal adduct prepared above were added. Subsequently an amount of 9,9-bis(methoxymethyl)fluorene corresponding to ~~0,200~~0.200 moles per mole of Mg, were added to the suspension. The temperature was raised to 100°C and maintained for 60 min. Then, the stirring was discontinued, the solid product was allowed to settle at 65°C for 15 minutes and the supernatant liquid was siphoned off.

Please replace the paragraph beginning at page 13, line 15, and ending at page 14, line 5, with the following paragraph.

Table 1

Ex.	MgCl ₂ • (ROH) _m (H ₂ O) _p		Synthesis Conditions			Support analysis				
	<i>m</i>	<i>P</i>	<i>LB</i>	<i>Mg/LB</i> (mol/mol)	<i>T</i> (°C)	<i>Mg</i> (Wt%)	<i>LB</i> (Wt%)	<i>EtOH</i> (Wt%)	<i>LB/Mg</i> (mol/mol)	<i>EtOH/Mg</i> (mol/mol)
1	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	DIPS	<u>1,251.25</u>	58	<u>14,014.</u> <u>0</u>	<u>8,38.3</u>	<u>30,930</u> <u>9</u>	<u>0,10.1</u>	<u>1,21.2</u>
2	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	EA	<u>1,251.25</u>	58	<u>15,315.</u> <u>3</u>	<u>5,85.8</u>	<u>33,433</u> <u>4</u>	<u>0,10.1</u>	<u>1,11.1</u>
3	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	EA	<u>0,900.90</u>	25	<u>15,415.</u> <u>4</u>	<u>5,75.7</u>	<u>33,833</u> <u>8</u>	<u>0,10.1</u>	<u>1,11.1</u>
4	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	Acetone	<u>2,502.50</u>	25	<u>15,215.</u> <u>2</u>	<u>4,44.4</u>	<u>31,531</u> <u>5</u>	<u>0,10.1</u>	<u>1,11.1</u>
5	<u>0,70</u> <u>7</u>	<u>0,160.16</u>	THF	<u>0,770.77</u>	58	<u>12,712.</u> <u>7</u>	<u>37,137.</u> <u>1</u>	<u>14,914</u> <u>9</u>	<u>1,01.0</u>	<u>0,60.6</u>
6	<u>0,70</u> <u>7</u>	<u>0,160.16</u>	THF	<u>2,502.50</u>	50	<u>16,916.</u> <u>9</u>	<u>15,715.</u> <u>7</u>	<u>21,021</u> <u>0</u>	<u>0,30.3</u>	<u>0,60.6</u>
7	<u>0,70</u> <u>7</u>	<u>0,160.16</u>	THF	<u>1,251.25</u>	58	<u>13,613.</u> <u>6</u>	<u>29,529.</u> <u>5</u>	<u>17,317</u> <u>3</u>	<u>0,70.7</u>	<u>0,70.7</u>
8	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	THF	<u>1,251.25</u>	58	<u>13,113.</u> <u>1</u>	<u>22,922.</u> <u>9</u>	<u>27,727</u> <u>7</u>	<u>0,60.6</u>	<u>1,11.1</u>
9	<u>1,81</u> <u>8</u>	<u>0,140.14</u>	THF	<u>1,251.25</u>	58	<u>12,012.</u> <u>0</u>	<u>16,416.</u> <u>4</u>	<u>41,041</u> <u>0</u>	<u>0,50.5</u>	<u>1,81.8</u>
10	<u>1,21</u> <u>2</u>	<u>0,150.15</u>	THF	<u>1,251.25</u>	50	<u>13,813.</u> <u>8</u>	<u>17,817.</u> <u>8</u>	<u>29,229</u> <u>2</u>	<u>0,40.4</u>	<u>1,11.1</u>
11	<u>1,81</u> <u>8</u>	<u>0,140.14</u>	THF	<u>2,502.50</u>	58	<u>12,912.</u> <u>9</u>	<u>4,34.3</u>	<u>43,943</u> <u>9</u>	<u>0,10.1</u>	<u>1,81.8</u>

Please replace the paragraph beginning at page 15, line 10, and ending at page 16, line 3, with the following paragraph.

Table 2

Catalyst synthesis			Catalyst composition				Catalyst performances		
Ex.	Adduct of Ex	Preparation Procedure	Ti (Wt%)	Mg (Wt%)	Cl (Wt%)	I. D. (Wt%)	Yield (Kg _{pol} /g _{cat})	X.I. (Wt%)	BDP (g/cm ³)
17	1	A	3,63.6	17,817.8	61,461.4	5,05.0	23,023.0	97,297.2	0,4320.43
18	2	B	3,83.8	16,816.8	60,060.0	8,48.4	32,032.0	84,884.8	0,4090.40
19	3	A	2,82.8	19,519.5	65,065.0	8,48.4	37,037.0	96,996.9	0,4200.42
20	4	A	2,82.8	19,919.9	67,767.7	7,67.6	38,038.0	97	0,3920.39
21	5	A	2,62.6	18,918.9	64,364.3	10,310.3	59,159.1	97,897.8	0,4310.43
22	6	A	4,34.3	17,817.8	64,264.2	2,72.7	17,317.3	97,097.0	0,4090.40
23	7	A	2,72.7	15,715.7	54,054.0	15,115.1	32,032.0	97,497.4	0,4510.45
24	8	A	3,23.2	19,619.6	65,065.0	6,76.7	65,365.3	98,498.4	0,3480.34
25	9	A	2,92.9	16,816.8	56,856.8	12,612.6	56,156.1	97,997.9	0,4500.45
26	6	B	1,61.6	16,416.4	53,053.0	7,37.3	9,39.3	94,394.3	-
27	7	B	2,42.4	19,319.3	63,663.6	7,47.4	55,255.2	96,996.9	0,4420.44
28	10	B	3,73.7	15,815.8	55,255.2	10,610.6	49,549.5	92,792.7	0,4100.41
29	8	B	3,83.8	15,215.2	54,454.4	11,711.7	66,166.1	95,695.6	0,3790.37
30	9	B	4,14.1	15,015.0	53,353.3	16,116.1	107,2107.2	97,897.8	0,4450.44
31	12	B	4,34.3	14,414.4	52,752.7	18,118.1	107,6107.6	97,697.6	0,3820.38

32*	13	A	<u>3,33.3</u>	<u>56,756.7</u>	<u>55,155.</u> <u>1</u>	<u>14,814.8</u>	<u>10,310.3</u>	<u>93,293.2</u>	-
33*	14	A	<u>2,42.4</u>	<u>20,620.6</u>	<u>66,166.</u> <u>1</u>	<u>5,35.3</u>	<u>25,125.1</u>	<u>95,895.8</u>	<u>0,3570.35</u> <u>7</u>
34*	15	A	<u>3,23.2</u>	<u>18,718.7</u>	<u>63,963.</u> <u>2</u>	<u>9,99.9</u>	<u>41,641.6</u>	<u>97,597.5</u>	<u>0,4360.43</u> <u>6</u>
35*	13	B	<u>2,22.2</u>	<u>18,918.9</u>	<u>61,561.</u> <u>5</u>	<u>3,83.8</u>	<u>6,46.4</u>	<u>75,375.3</u>	-
36*	14	B	<u>6,06.0</u>	<u>16,416.4</u>	<u>61,761.</u> <u>7</u>	<u>11,711.7</u>	<u>24,124.1</u>	<u>73,073.0</u>	-
37*	15	B	<u>5,35.3</u>	<u>15,615.6</u>	<u>58,258.</u> <u>2</u>	<u>7,27.2</u>	<u>62,362.3</u>	<u>92,592.5</u>	<u>0,4080.40</u> <u>8</u>
38*	16	B	<u>4,94.9</u>	<u>15,415.4</u>	<u>59,259.</u> <u>2</u>	<u>10,610.6</u>	<u>88,988.9</u>	<u>96,096.0</u>	<u>0,4030.40</u> <u>3</u>